## **UNIC DF Training**

Gas Properties



### Natural gas

- Naturally occurring mixture of gaseous saturated hydrocarbons
- Is found in layers of porous rock, like limestone or sandstone beneath the earth's surface, often in association with crude oil
- Has high heating value and clean burning characteristics
- Heavier hydrocarbons in natural gas can be extracted through compression or absorption processes to yield butane, propane, gasoline and other raw material for petrochemical industry





### Abbreviations

| Abbreviation | Meaning                   | Remarks   |
|--------------|---------------------------|---|
| NG           | Natural Gas               |   |
| LNG          | Liquefied Natural Gas     | Liquid state.<br>Cold, -163°C.<br>Usually stored in 0 bar to 10 bar<br>pressure                     |
| CNG          | Compressed Natural<br>Gas | Compressed gas<br>Usually pressurized to 200-250 bar<br>Temperature can be increased<br>(to -25°C). |
| PNG          | Pressurized Natural Gas   | As CNG  |



- Natural gas is mostly methane (CH<sub>4</sub>).
- Methane contains the higher amount of hydrogen per unit of energy than any other fossil fuel.
- Carbon to hydrogen ratio 1 / 4 (gasoline: 1 / 2.25).
- Lower CO<sub>2</sub> emissions



### Gas composition

The composition of the natural gas varies substantially between the various at production fields.

| Property          | Volume                        |            |
|-------------------|-------------------------------|------------|
| Methane           | CH <sub>4</sub>               | 70 – 90 %  |
| Ethane            | $C_2H_6$                      | 0 – 7 %    |
| Propane           | C <sub>3</sub> H <sub>8</sub> | 0 – 2 %    |
| Butane            | $C_4H_{10}$                   | 0 – 0,5 %  |
| Hydrogen          | H <sub>2</sub>                | Traces     |
| Carbon dioxide    | CO <sub>2</sub>               | 0 – 10 %   |
| Oxygen            | 02                            | 0 – 0.2 %  |
| Nitrogen          | $N_2$                         | 0 – 15 %   |
| Hydrogen sulphide | H <sub>2</sub> S              | 0 – 10 ppm |
|                   |                               |            |

Trace amounts of chlorine, fluorine, ammonia, hydrogen sulphide, particles.



| Table 4-10 Ga | s specifications |
|---------------|------------------|
|---------------|------------------|

| Property                                 | Value<br>(values given in Nm <sup>3</sup> are at 0 °C and 101.3 kPa)                         |
|--|--|
| Lower heating value (LHV)                | $\geq$ 28 MJ/Nm <sup>3</sup>   |
| Influence of MN on max. eng. output      | See graph in 1.5 Operation in gas mode, 🗎 1-6.   |
| Methane content                          | ≥70% volume  |
| Hydrogen sulphide (H <sub>2</sub> S)     | ≤0.05% volume  |
| Hydrogen (H <sub>2</sub> ) <sup>a)</sup> | ≤3% volume   |
| Ammonia                                  | ≤25 mg/Nm <sup>3</sup>   |
| Chlorine and fluorine                    | $\leq$ 50 mg/Nm <sup>3</sup>   |
| Water (vapour pressure dew-point)        | ≤ -20 °C   |
| Oil (aerosol liquid and vapour)          | ≤1mg/Nm <sup>3</sup>   |
| Gas cleanliness                          | Gas is considered as sufficiently clean. b)  |
| Gas temperature at GVU inlet             | 20-60 °C at normal condition<br>0-20 °C exceptionally for short-time operation <sup>c)</sup> |
| Gas feed pressure <sup>d)</sup>          | According to GTD   |
| Permissible gas pressure fluctuation     | ±0.6bar (across all frequencies)   |

a) Hydrogen content higher than 3% volume must be considered on a project-specific basis.

- b) Contamination from gas system has to be avoided, e.g. by correct pipe flushing, ensuring cleanliness of bunkering connections, etc.
- c) For instance, during starting-up of the fuel gas supply system.



Properties of pure methane

- Density
- Boiling point
- Lower heating value
- Explosion limits 5 14 % mole
- Auto-ignition temperature 630 ° C
- Methane Number(Knock Resistance) : 100
- Reference values for auto-ignition temperatures of other gases:

- 161.5 °C

48,0-50,0 MJ/kg

| • | Ethane ( $C_2H_6$ )  | 515 °C |
|---|----------------------|--------|
| • | Propane ( $C_3H_8$ ) | 480 °C |

• Butane (C<sub>4</sub>H<sub>10</sub>) 420 °C

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0.7175 kg/m<sup>3</sup> @ 1.01325 bar and 0 °C

### Properties of pure ethane

• Density

1.282 kg/m<sup>3</sup> @ 15 °C gas, 1 atm

- Boiling point
- Lower heating value 61,0-63,0 MJ/kg
- Explosion limits 3 13 % mole
- Auto-ignition temperature 515 ° C
- Methane Number(Knock Resistance) : 44
- Reference values for auto-ignition temperatures of other gases:

- 89 ° C

| • | Methane (CH <sub>4</sub> ) | 630 °C |
|---|----------------------------|--------|
| • | Propane ( $C_3H_8$ )       | 480 °C |

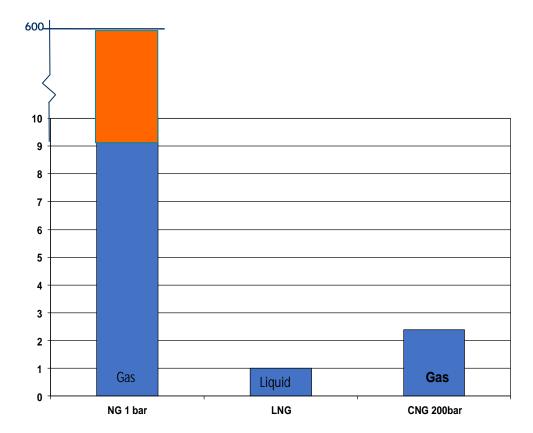
• Butane (C<sub>4</sub>H<sub>10</sub>) 420 °C



### Liquefied natural gas

- LNG takes up about 1/600th the volume of natural gas in the gaseous state.
- LNG is principally used for transporting natural gas to markets, where it is re-gasified and distributed as pipeline natural gas.
- Its relatively high cost of production and the need to store it in expensive cryogenic tanks have prevented its widespread use in commercial applications.

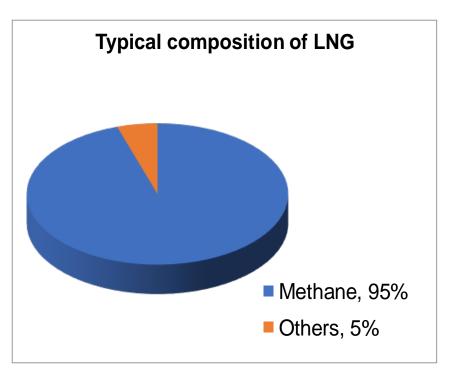
#### Fuel relative volume, energy content equal



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### LNG properties

- The density of LNG is roughly 0,4 kg/L to 0,5 kg/L, depending on temperature, pressure and composition, compared to water at 1,0 kg/L.
- The energy density of LNG is comparable to propane and ethanol but is only 60% that of diesel and 70% that of gasoline.

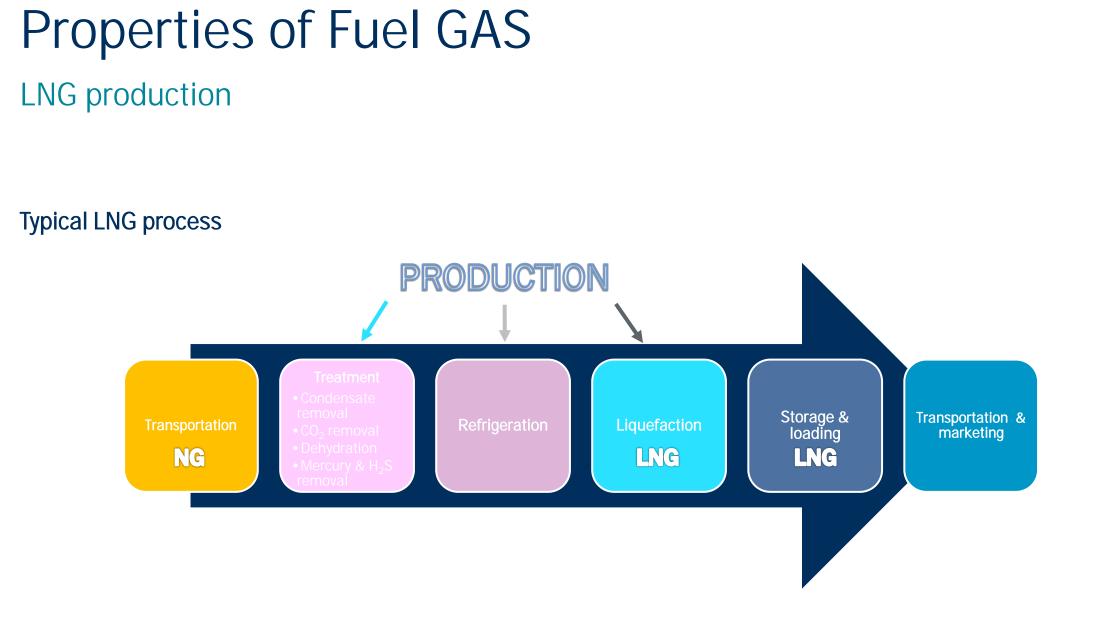




LNG properties

- Narrow ignition area.
- High self-ignition temperature (> 500 °C).
- Slow flame rate in atmospheric pressure.
- LNG does not burn, it has to evaporate first.
- Ignition energy is low, i.e. a small spark is enough.



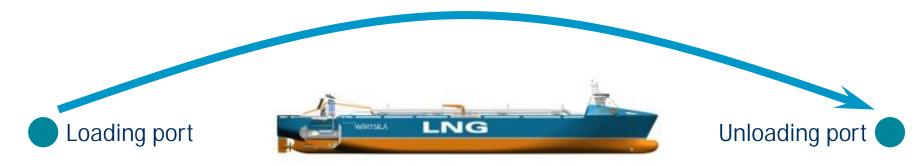




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Change in gas composition during voyage

After loading: LNG very cold (e.g. -163  $^{\circ}$  C) N<sub>2</sub> evaporates first **Before unloading:** LNG temperature rises Possible excess of NBOG

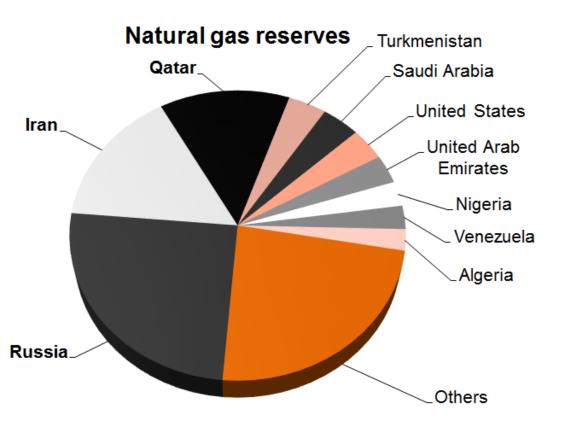




LNG production

A majority of the world's LNG supply comes from countries with large natural gas reserves:

- Russia
- Iran
- Qatar
- Turkmenistan
- Saudi-Arabia
- United States
- United Arab Emirates
- Nigeria
- Venezuela
- Algeria

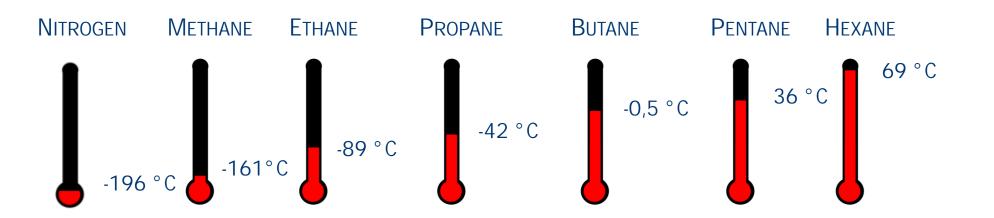




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### Natural Boil-Off Gas composition

- LNG is not stable in ambient conditions
- Heat is constantly transferred through LNG containment walls:
  - The LNG will start evaporate creating Natural Boil-Off Gas (NBOG)
  - In the beginning of the process, components with lower boiling point will start evaporating first.
  - Forced Boil-Off Gas (FBOG) is simply LNG evaporated through a heat exchanger





### Lower heating value

- Lower Heating Value corresponds to the energy content of the gas.
- If the LHV is lower than specified, the engine output has to be adjusted or a higher gas pressure to the engine is needed.
- To compensate low heating value:
  - Higher gas feed pressure
  - Derating of engine output



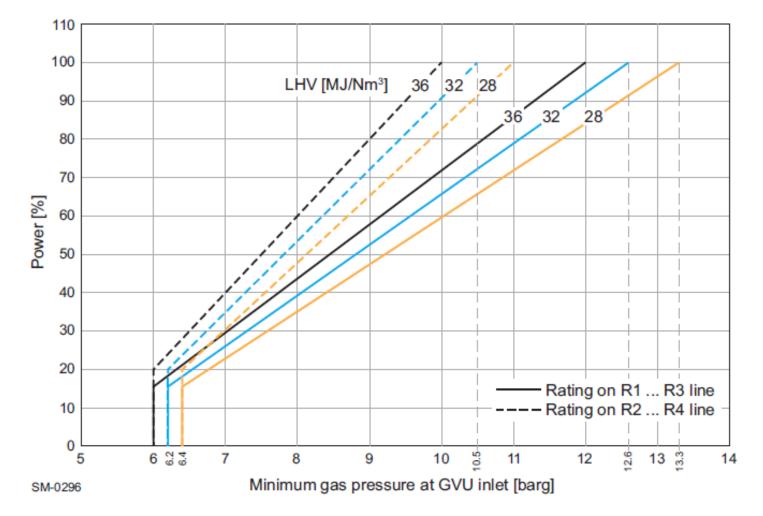


Figure 4-21 Design gas feed pressure requirements



### Methane number (MN)

- Is a scale for evaluation of the knock (auto-ignition) resistance of the fuel.
- Higher MN means better knock resistance.
- Can be calculated, when gas composition is known.
- Higher amount of heavier hydrocarbons decrease MN.
- Higher amount of carbon dioxide and nitrogen increase MN.
- If MN is too low, the engine derating is required.



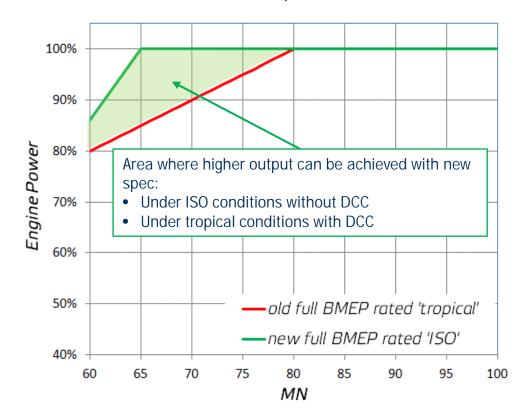
### Methane number (MN)

- MN is as a measure for knock sensitivity, like Octane numbers for petrol fuel. CH<sub>4</sub> (methane) has MN = 100, H<sub>2</sub> (hydrogen) has MN = 0. Heavier hydrocarbons decreases MN. Inert gases (CO<sub>2</sub> and N<sub>2</sub>) increases MN.
- WinGD derating rules are based on MN.



Power de-rating – Methane Number under tropical condition and ISO condition

Maximum achievable power





#### Heavier hydrocarbons

Heavier hydrocarbons can condense in gas compressor. The higher the amount of heavier HCs, the lower the MN. If the amount of heavier hydrocarbons ( $C_4$ +) in natural gas is above 1 %, the risk of knocking increases.

#### Hydrogen

Increases the risk of pre-ignition during a compression stroke. Decreases density, MN and LHV (volume basis) of natural gas. Sets new challenges to the controlled combustion process. Increases explosion risk.



### Hydrogen sulphide

- Causes sulphide stress corrosion
- Severity of corrosion depends on gas pressure (higher pressure, higher risk)
- Correct material choices will decrease the corrosion risk

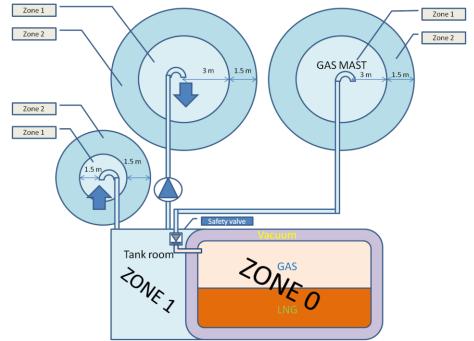


### Marine safety regulations

- International Convention for the Safety of Life at Sea (SOLAS) rules will have references to the IGF Code
- IGC Code (International Gas Carrier Code)
- IMO IGF Code (Code of Safety for Gas-fuelled Ships)
- IMO MSC adopted the Interim Guidelines on safety for natural gas-fuelled engine installations in ships (resolution MSC-285(86))
- DNV-GL rules are available



### Gas Dangerous Zones (GDZ)



| Three levels of hazardous zones defined as per IGF Code |   |
|---|---|
| Hazardous area zone 0                                   | <ul> <li>All areas where gas is present i.e. inside gas tank and gas pipes</li> </ul>         |
| Hazardous area zone 1                                   | <ul> <li>All areas where gas might be present</li> </ul>                                      |
| Hazardous area zone 2                                   | <ul> <li>All areas within 1,5 m surrounding open or semi-enclosed spaces of zone 1</li> </ul> |

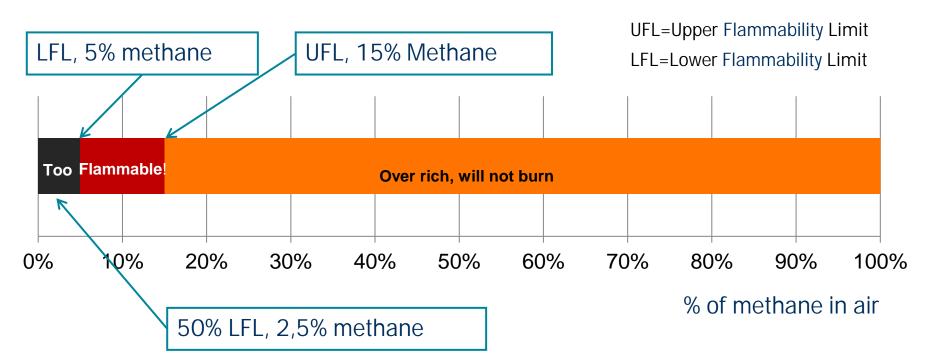


### Safety

- Natural gas is flammable and highly explosive in suitable conditions.
- Natural gas is lighter than air -opposite to liquefied petroleum gases propane and butane.
- Odorant is added to natural gas in order to detect possible leakage. e.g. *Tetrahydrothiophene (THT, C\_4H\_8S)*
- Burning of natural gas gives water and carbon dioxide.
- Incomplete burning gives toxic carbon monoxide.
- Risk of freezing hazard.
- Safety clothing & equipment.



### Flammability limits

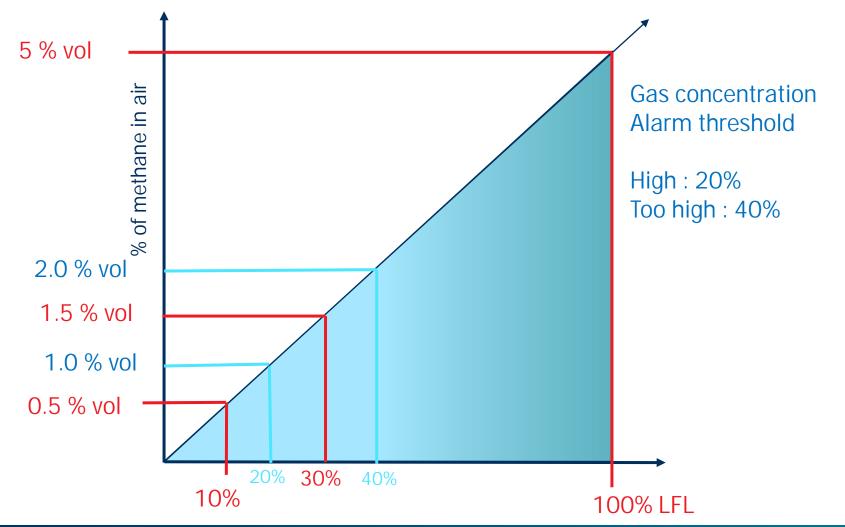


In WinGD gas applications:

- Pipe leaks are ventilated, mixture stays too lean for ignition (Marine installation approach).
- Storage tanks have a too rich environment for ignition.



### WinGD typical alarm levels





### The presence of gas

There is always the possibility of the presence of gas in the atmosphere, particularly:

- During bunkering of liquefied gases
- During loading and unloading of liquefied gases
- During the maintenance of the gas feed and storing systems
- Venting gas area near to gas mast



### LNG leakage

- In ambient temperature the LNG quickly vaporizes to gaseous form.
- In case of leakage of the LNG there is a risk for exposure to methane.
- Large concentrations of methane gas can cause suffocation as methane can drive away oxygen.
- Rapid evaporation of LNG can cause freezing injuries.



### LNG spill

- If liquefied natural gas is spilled onto ship's deck or over the side of the ship constructed of traditional steel, because of evaporation the deck or ship side will cool down to a temperature that is well below the temperature of the liquid.
- If the spill is large it may result a fracture of the ship's hull or deck.
- Due to the reasons mentioned above, when handling very low temperature liquids like LNG, wooden of stainless steel drip trays are normally provided under the ship's bunkering station.



### 2S DF proactive approach to safety

#### Monitoring – Detection

- Safety sequences performed by Engine Control System and Gas Valve Unit
- Gas detectors
- Pressure sensors

#### Containment - Leak prevention

- Double walled piping Enclosed type Gas Valve Unit
- Automatic shut-off valves before engine room inlet/in iGPR or GVU/on gas manifold
- Gas vent valves

#### Additional safety measures

- Purging with inert gas
- Forced ventilation of exhaust piping
- Explosion protection devices on exhaust gas system



### Conclusions

LNG is as safe as any other fuel when:

- its distinct properties and handling particularities are known and considered
- the relevant safety precautions are observed
- the right procedures are followed

2S DF engines and fuel gas handling systems are designed to:

- Monitor & detect
- Warn
- Prevent
- Contain

Everyone is personally responsible for their own safety and the safety of others.

Always think before acting and when in doubt, ASK

